



(19)

Europäisches Patentamt
European Patent Office
Office européen des brevets



(11)

EP 0 525 844 B1

(12)

EUROPEAN PATENT SPECIFICATION

(45) Date of publication and mention
of the grant of the patent:
26.11.1997 Bulletin 1997/48

(51) Int Cl.⁶: **C22C 29/12, C22C 32/00,**
H01M 8/12, C22C 1/10

(21) Application number: **92201698.5**

(22) Date of filing: **11.06.1992**

(54) **Nickel cermet, and process for preparing it**

Nickel-Cermet und Verfahren zur seiner Herstellung

Cermet en nickel et procédé de fabrication

(84) Designated Contracting States:
AT BE CH DE DK ES FR GB GR LI LU MC NL PT
SE

(30) Priority: **28.06.1991 IT MI911792**

(43) Date of publication of application:
03.02.1993 Bulletin 1993/05

(73) Proprietors:
• **ENIRICERCHE S.p.A.**
20121 Milano (IT)
• **SNAM S.p.A.**
I-20121 Milan (IT)

(72) Inventors:
• **Lockhart, Thomas Paul**
I-20075 Lodi, Milan (IT)
• **Piro, Giampaetro**
I-20134 Milan (IT)

• **Gagliardi, Federica**
I-21053 Castellanza (Varese) (IT)
• **Zanibelli, Laura**
I-20161 Milan (IT)

(74) Representative: **Fusina, Gerolamo et al**
Ing. Barzanò & Zanardo Milano S.p.A,
Via Borgonuovo, 10
20121 Milano (IT)

(56) References cited:
DE-A- 2 806 408 GB-A- 919 052
US-A- 3 085 876

• **JOURNAL OF THE ELECTROCHEMICAL**
SOCIETY. vol. 137, no. 10, October 1990,
MANCHESTER, NEW HAMPSHIRE US pages
3042 - 3047 TATSUYA KAWADA ET AL
'Characteristics of Slurry-Coated Nickel Zirconia
Cermet Anodes for Solid Oxide Fuel Cells'

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid. (Art. 99(1) European Patent Convention).

EP 0 525 844 B1

Description

The present invention relates to a nickel cermet, to the process for preparing it and to the use thereof as anodic material for solid oxide fuel cells (SOFC).

Solid oxide fuel cells (SOFC) are known in the art, which use, as solid electrolyte, a mixture of yttria (Y_2O_3) and zirconia (ZrO_2), an anode formed by a nickel/zirconia cermet and a lanthanum manganite ($LaMnO_3$) cathode. For a general description of such cells, reference is made to Ullmann's Encyclopedia of Industrial Chemistry, Vol. A12, Ed. 1989, pages 80-82 and to the references cited therein.

The nickel/zirconia cermet used as the anodic material is normally constituted by a dispersion of nickel metal in zirconia stabilized in the cubic crystal form with yttria.

The processes for preparing such a cermet essentially comprise mechanically dispersing nickel oxide throughout the stabilized zirconia, then reducing nickel oxide into nickel metal. So, e.g., according to the specification of U.S. 3,300,344; mixed zirconia and yttria, obtained by precipitation from an aqueous solution, are transformed into shaped bodies with the addition of nickel oxide and carbon powder, and the nickel oxide is reduced in order to yield nickel metal, owing to the effect of carbon powder at high temperature.

Furthermore, in the paper: Morphology and Electrochemistry of Porous Nickel/Zirconia Cermets, at pages 90-98 of Proceedings of the First International Symposium on Solid Oxide Fuel Cells, S.C. Singhal, Ed. 1989, the reduction with hydrogen of a mixture of sintered powders obtained by co-milling, with a ball mill, nickel oxide and stabilized zirconia, is described. Other well-known techniques are those based on C.V.D. (chemical vapour deposition) and P.S. (plasma spraying) described, e.g., by H. Arai in International Symposium on SOFC, Nov. 13-14th, 1989, Nagoya, Japan.

The nickel cermets obtained by means of the processes known from the prior art are not completely satisfactory in the application to fuel cells, mainly due to their incapability to supply nickel with a large enough active surface-area for offering interesting catalytic properties (A.L. Lee et al., Ind. Eng. Chem. Res., 1990, 29, 766-773).

Another problem derives from the difficulty of accomplishing a complete reduction of nickel oxide particles, into nickel metal. The paper by S.C. Singhal, cited hereinabove, reports in fact that the particles with larger size than approximately $3\text{ }\mu\text{m}$ retain an NiO core after their reduction with hydrogen. On the other hand, as regards the C.V.D. and P.S. techniques, problems exist as to the quality of the resulting material and due to the difficulties to be faced when said techniques are applied to the construction of medium- and high-power cells.

The present Applicant found now, according to the present invention, a process which makes it possible a solid material composed by nickel oxide and stabilized zirconia, as two distinct phases, with a phase distribution at a lower level than $1\text{ }\mu\text{m}$, to be obtained.

It was furthermore found that nickel oxide contained in such a solid material can be reduced to a complete, or substantially complete, extent, by means of hydrogen, in order to yield a nickel cermet with a submicronic distribution of the phases and a large active nickel surface-area, so as to render the same cermet particularly suitable for use as material for solid oxide fuel cells (SOFC).

In accordance therewith, according to an aspect thereof, the present invention relates to a nickel cermet consisting of 35-70% by weight of a metal nickel phase and 65-30% by weight of a zirconia phase stabilized in the cubic form with yttria, with, on X-ray diffraction analysis, both said phases appearing as distinct and homogeneously distributed at a level lower than $1\text{ }\mu\text{m}$, and said nickel cermet, when submitted to the hydrogen chemisorption test by means of the pulsed technique, showing a percent dispersion of nickel of from 0.2 to 2.0 and a specific surface-area comprised within the range of from 2 to $12\text{ m}^2/\text{g}$ of nickel and of from 1 to $4\text{ m}^2/\text{g}$ of cermet.

Such a nickel cermet usually displays a portion of its surface-area coated with nickel, which is comprised within the range of from 4 to 30%, or even more, of its total surface-area.

According to another aspect thereof, the present invention relates to a process for preparing a nickel cermet with the above reported characteristics, which process comprises the following steps:

- (a) preparing an aqueous solution containing a water-soluble, heat-decomposable zirconyl, yttrium and nickel salt, and an organic hydroxyacid or aminoacid, or a poly(acrylic acid);
- (b) removing water from the solution prepared in above step (a), in the absence, or in the substantial absence, of decomposition phenomena, in order to separate a porous solid material;
- (c) calcining the porous solid separated in the step (b), under oxidizing conditions, in order to cause the formation to occur of a solid material containing two distinct phases of nickel oxide, and of zirconia stabilized in the cubic form with yttria, with a phase distribution at a lower level than $1\text{ }\mu\text{m}$; and
- (d) reducing the nickel oxide into nickel metal, inside the solid material obtained from the step (c), in order to obtain the nickel cermet.

The water-soluble, heat-decomposable salts of zirconyl, yttrium and nickel used in order to prepare the solution in the step (a) of the present process can be selected from among the salts of carboxy acids, or nitrate salts. Particularly

suitable salts are zirconyl nitrate, zirconyl acetate, yttrium acetate, nickel nitrate and nickel acetate. The hydroxyacids suitable for use in the present invention are selected from among aliphatic or aromatic hydroxyacids, such as citric acid, lactic acid, glycolic acid, tartaric acid and mandelic acid. Of these, citric acid is preferred.

Suitable aminoacids are glycine and alanine. For the intended purpose, also a poly(acrylic acid) may be used.

Advantageously, aqueous solutions of zirconyl, yttrium and nickel salts are prepared, in which the relative ratios of the same salts are such as to have, in the nickel cermet obtained as the end product, from 35 to 70% by weight of nickel metal and from 65 to 30% by weight of zirconia stabilized with from 5 to 20 mol of yttria per each 100 mol of zirconia. The amount of organic hydroxyacid or aminoacid may furthermore be comprised within the range of from 2 to 4 mol per each mol of zirconium, yttrium and nickel metals. Under these conditions, the pH of the solution will normally be comprised within the range of from 2 to 5.

The solution can be prepared by dissolving in water the salts and the organic hydroxyacid, operating at room temperature, or favouring the solubilization by operating at higher temperatures. The order of addition of the reactants is not critical; however, forming an aqueous solution of the organic hydroxyacid and adding to said solution the salts of zirconyl, yttrium and nickel, is preferable.

According to the present invention, from the resulting solution water is removed, in the step (b) of the process, by operating under such temperature conditions as to prevent, or substantially prevent, any decomposition phenomena. In particular, said water removal can be carried out by evaporating water under vacuum, at a temperature not higher than about 80°C, by working, e.g., on a rotational evaporator.

According to an alternative operating way, water is removed by means of the spray-drying technique, by feeding the solution, with a concentration of from about 5 to about 30% (by weight/weight), in a finely subdivided form, to an apparatus for co-current or counter-current spray-drying with an inert gas, such as nitrogen, or air.

In general, the gas stream entering the spray dryer should have a temperature comprised within the range of from 150°C to 300°C, preferably of from 180°C to 200°C, and the leaving stream should preferably have a temperature of the order of from 90°C to 200°C, preferably of from 130°C to 170°C. In any case, from the drying step a crumbly, porous solid, generally of green-ochre colour -- according to the temperature values used -- will be obtained.

According to the present invention, the solid material obtained in that way is submitted to calcination, in the step (c) of the present process, by operating at high temperatures and in an oxidizing atmosphere. In particular, suitable calcination temperatures are generally comprised within the range of from 800°C to 1000°C, and the calcination times should generally be comprised within the range of from 1 to 10 hours. According to a preferred form of practical embodiment, the calcination is carried out at temperatures of the order of 900°C, for a time of from 3 to 5 hours. The oxidizing atmosphere can be constituted by oxygen, air, or oxygen-enriched air. By operating under these conditions, from the solid material the combustible or decomposable fraction is removed, and the formation of the oxides of the metals present is caused. Surprisingly, it was observed that such a solid material consists of two distinct phases of nickel oxide and zirconia stabilized in the cubic form with yttria, with a phase distribution at a lower level than 1 µm.

This solid material is submitted to treatment with hydrogen, in the step (d) of the process, in order to reduce nickel oxide into nickel metal, and obtain the nickel cermet. In particular, the reduction is carried out by bringing the calcined solid material into contact with hydrogen gas, operating at temperatures comprised within the range of from 20°C to 1000°C, in order to obtain a complete, or substantially complete, reduction of nickel oxide into nickel metal. Useful reduction times are of the order of from 1 to 3 hours.

In that way, the nickel cermet according to the present invention is obtained, which generally contains 35-70% by weight of a metal nickel phase and 65-30% by weight of a zirconia phase stabilized in the cubic form with yttria, and displaying the other characteristics, as reported hereinabove.

According to a further aspect thereof, the present invention relates to a solid oxide fuel cell (SOFC) characterized in that it comprises, as its anode, the nickel cermet with the characteristics reported hereinabove.

In particular, such an anode can be obtained by applying, according to known techniques, the nickel cermet of the present invention to a solid electrolyte of zirconia stabilized with yttria.

According to a particular form of embodiment of the solid electrolyte, the powder of metal oxides obtained after calcination in the step (c) of the process is applied, followed by the reduction, *in situ*, of nickel oxide into nickel metal.

The following experimental examples are given for the purpose of better illustrating the present invention.

Example 1

In 330 ml of demineralized water, 100.07 g of citric acid monohydrate ($C_6H_8O_7 \cdot H_2O$) is dissolved at room temperature, and then 15.605 g of zirconyl nitrate hydrate $ZrO(NO_3)_2 \cdot xH_2O$ (zirconium content 32.71% by weight), 4.332 g of yttrium acetate tetrahydrate $Y(CH_3COO)_3 \cdot 4H_2O$ (26.8% by weight of yttrium) and 25.46 g of nickel nitrate hexahydrate $Ni(NO_3)_2 \cdot 6H_2O$ (20.18% by weight of nickel) are dissolved.

The solution is charged to a rotational evaporator and the solvent is evaporated by operating at 70°C and 74 mmHg. A 146 g of a crumbly, porous solid residue of green colour is collected.

The solid is calcined in a muffle at 900°C for 4 hours, under a flowing air stream. A 16.38 g of a solid material is collected which, on analysis by powder X-ray diffraction, results to be constituted by nickel oxide and zirconia stabilized with yttria, without other detectable crystalline phases. The nickel content in the solid product is of 35.14% by weight.

5 The calcined solid is furthermore submitted to an X-ray mapping (STEM) which allows the distribution of the crystalline phases present in the sample, to be examined at sub-micronic level.

It is thus determined that nickel oxide is uniformly distributed, at a level lower than 1 µm, throughout the matrix of zirconia stabilized with yttria.

The calcined solid material is submitted to reduction by means of TPR (Thermal Programmed Reduction) technique. More particularly 50 mg of sample, with particle size comprised within the range of from 20 to 40 mesh, is charged to a tubular quartz reactor and is exposed to a hydrogen stream flowing at a flowrate of 2.2 ml/minute, diluted in 17 ml/minute of helium (purity of gases 99.999%).

The sample is heated by means of a tubular furnace, using a linear thermal ramp of 10°C/minute, from 30 to 900°C. The effluent stream from the reactor is analysed by a quadrupolar mass spectrometer. The results of the reduction test are reported in Table I.

15 The hydrogenated sample is submitted to tests of hydrogen chemisorption by means of the pulsed technique.

From such test, the values are obtained of % nickel dispersion; of specific surface-area, as m²/g of nickel; of specific surface-area, as m²/g of cermet; and of coated surface-area, as % of total surface-area. These data are reported in Table II.

20 Example 2

In 250 ml of demineralized water, 38.8 g of citric acid monohydrate (C₆H₈O₇·H₂O) is dissolved at room temperature, and then 3.91 g of zirconyl nitrate hydrate ZrO(NO₃)₂·xH₂O (zirconium content 32.71% by weight), 1.08 g of yttrium acetate tetrahydrate Y(CH₃COO)₃·4H₂O (26.8% by weight of yttrium) and 12.73 g of nickel nitrate hexahydrate Ni(NO₃)₂·6H₂O (20.18% by weight of nickel) are dissolved.

25 The solution is charged to a rotational evaporator and the solvent is evaporated by operating at 70°C and 74 mmHg. 56.55 g of a crumbly, porous solid residue of green colour is collected, which is calcined in a muffle at 900°C for 4 hours, under a flowing air stream. A 5.73 g of a solid material is collected which, on analysis by powder X-ray diffraction, results to be constituted by nickel oxide and zirconia stabilized with yttria, without other detectable crystalline phases. The nickel content in the solid product is of 44.7% by weight.

30 The calcined solid is furthermore submitted to an X-ray mapping (STEM) which allows the distribution of the crystalline phases present in the sample, to be examined at sub-micronic level.

It is thus determined that nickel oxide is uniformly distributed, at a lower level than 1 µm, throughout the matrix of zirconia stabilized with yttria.

35 A sample of 50 mg of the calcined solid material, with particle size comprised within the range of from 20 to 40 mesh, is treated with hydrogen under the same conditions of Example 1. The results of the test are reported in Table I.

Example 3

40 In 250 ml of demineralized water, 27.07 g of citric acid monohydrate (C₆H₈O₇·H₂O) is dissolved at room temperature, and then 1.95 g of zirconyl nitrate hydrate ZrO(NO₃)₂·xH₂O (zirconium content 32.71% by weight), 0.54 g of yttrium acetate tetrahydrate Y(CH₃COO)₃·4H₂O (26.8% by weight of yttrium) and 8.54 g of nickel nitrate hexahydrate Ni(NO₃)₂·6H₂O (20.18% by weight of nickel) are dissolved.

45 The weight of the solution is adjusted at 500 g by means of the addition of distilled water. The resulting solution is sent to a spray dryer operating with an entering gas flow with the temperature of 215°C and a leaving gas flow with the temperature of 150°C. A 38.1 g of a crumbly, porous solid residue of green colour is collected, which is calcined in a muffle at 900°C for 4 hours, under a flowing air stream. A 3.78 g of a solid material is collected which, on analysis by powder X-ray diffraction, results to be constituted by nickel oxide and zirconia stabilized with yttria, without other detectable crystalline phases. The nickel content in the solid product is of 55.70% by weight.

50 The calcined solid is furthermore submitted to an X-ray mapping (STEM) which allows the distribution of the crystalline phases present in the sample, to be examined at sub-micronic level.

It is thus determined that nickel oxide is uniformly distributed, at a level lower than 1 µm, throughout the matrix of zirconia stabilized with yttria.

55 A sample of 50 mg of the calcined solid material, with particle size comprised within the range of from 20 to 40 mesh, is treated with hydrogen under the same conditions of Example 1. The results obtained from this test are reported in Table I.

A sample of 0.4548 g of hydrogenated solid material is submitted to chemisorption tests as described in Example 1, and the results are reported in Table II.

Table I

Example No.	T(°C) of reduction beginning	T(°C) of reduction end	T(°C) at which reduction rate is maximal
1	322	454	398
2	288	468	398
3	305	498	405

Table II

Example No.	Dispersion (Ni %)	Specific surface-area, m ² /g of Ni	Specific surface-area, m ² /g of solid	Coated surface, %
1	1.4903	9.9278	3.4886	21.05
2	0.5122	3.4121	1.900	18.55
3	0.8708	5.808	2.7670	19.60

Claims

- Nickel cermet consisting of 35-70% by weight of a metal nickel phase and 65-30% by weight of a zirconia phase stabilized in the cubic form with yttria, with, on X-ray diffraction analysis, both said phases appearing as distinct and homogeneously distributed at a level lower than 1 μm , and said nickel cermet, when submitted to the hydrogen chemisorption test by means of the pulsed technique, showing a percent dispersion of nickel of from 0.2 to 2.0 and a specific surface-area comprised within the range of from 2 to 12 m²/g of nickel and of from 1 to 4 m²/g of cermet.
- Process for preparing the nickel cermet according to claim 1, characterized in that said process comprises the following steps:
 - preparing an aqueous solution containing a water-soluble, heat-decomposable zirconyl, yttrium and nickel salt, and an organic hydroxyacid or aminoacid, or a poly(acrylic acid);
 - removing water from the solution prepared in above step (a), in the absence, or in the substantial absence, of decomposition phenomena, in order to separate a porous solid material;
 - calcining the porous solid separated in the step (b), under oxidizing conditions, in order to cause the formation to occur of a solid material containing two distinct phases of nickel oxide, and of zirconia stabilized in the cubic form with yttria, with a phase distribution at a level lower than 1 μm ; and
 - reducing the nickel oxide into nickel metal, inside the solid material obtained from the step (c), in order to obtain the nickel cermet.
- Process according to claim 2, characterized in that the water-soluble, heat-decomposable zirconyl, yttrium and nickel salts, used to form the solution in the step (a), are selected from among the salts of carboxy acids, or nitrate salts.
- Process according to claim 3, characterized in that said zirconyl, yttrium and nickel salts are zirconyl nitrate, zirconyl acetate, yttrium acetate, nickel nitrate and nickel acetate.
- Process according to claim 2, characterized in that the organic hydroxyacids are selected from among citric acid, lactic acid, glycolic acid, tartaric acid and mandelic acid and the organic aminoacids are selected from glycine and alanine.
- Process according to claim 5, characterized in that the hydroxyacid used is citric acid.
- Process according to claims from 2 to 6, characterized in that in the step (a) an aqueous solution of zirconyl, yttrium and nickel salts is prepared with such relative ratios of the same salts as to have, in the nickel cermet obtained as the end product, a content of from 35 to 70% by weight of nickel metal and from 65 to 30% by weight of zirconia stabilized with from 5 to 20 mol of yttria per each 100 mol of zirconia, with the amount of organic hydroxyacid or aminoacid being comprised within the range of from 2 to 4 mol per each mol of zirconium, yttrium and nickel metals,

and the pH value of the solution being comprised within the range of from 2 to 5.

8. Process according to claim 2, characterized in that in the step (b) water is removed from the solution by operating under vacuum at a temperature not higher than about 80°C or by spray-drying.
9. Process according to claim 2, characterized in that in the step (c) the calcination is carried out at a temperature comprised within the range of from 800°C to 1000°C, during a time of from 1 to 10 hours in an atmosphere of oxygen, air, or oxygen-enriched air.
10. Process according to claim 9, characterized in that said calcination is carried out at about 900°C during a time of from 3 to 5 hours.
11. Process according to claim 2, characterized in that in the step (d) the reduction is carried out by bringing the calcined solid material into contact with hydrogen gas, operating at temperatures comprised within the range of from 20°C to 1000°C.
12. Use of nickel cermet according to claim 1, as anodic material for solid oxide fuel cells (SOFC).

Patentansprüche

1. Nickelcermet bestehend aus 35-70 Gew.-% einer Metalnichelphase und 65-30 Gew.-% einer Zirkoniumdioxidphase, die in der kubischen Form mit Yttriumoxid stabilisiert ist, wobei in der Röntgenbeugungsanalyse beide Phasen getrennt und homogen verteilt erscheinen auf einem Niveau unter 1 µm und das Nickelcermet, wenn es dem Wasserstoff-Chemisorptionstest mit Hilfe der Impulstechnik unterworfen wird, eine prozentuale Dispersion des Nickel von 0,2 bis 2,0 und eine spezifische Oberfläche im Bereich von 2 bis 12 m²/g des Nickels und von 1 bis 4 m²/g des Cermets zeigt.
2. Verfahren zur Herstellung des Nickelcermets nach Anspruch 1, gekennzeichnet durch die folgenden Schritte:
 - (a) Herstellen einer wäßrigen Lösung, die ein wasserlösliches, durch Wärme zersetzliches Zirkoniumoxid-, Yttrium- und Nickelsalz sowie eine organische Hydroxysäure oder Aminosäure oder Polyacrylsäure enthält;
 - (b) Entfernen des Wassers aus der in obiger Stufe (a) hergestellten Lösung ohne oder im wesentlichen ohne Zersetzungserscheinungen, um ein poröses, festes Material abzutrennen;
 - (c) Calcinieren des in der Stufe (b) abgetrennten porösen, festen Materials unter oxidierenden Bedingungen, um die Bildung eines festen Materials stattfinden zu lassen, das zwei getrennte Phasen des Nickeloxids und des in der kubischen Form mit Yttriumoxid stabilisierten Zirkoniumdioxids mit einer Phasenverteilung auf einem Niveau unter 1 µm enthält; und
 - (d) Reduzieren des Nickeloxids zu Nickelmetall innerhalb des in der Stufe (c) erhaltenen festen Materials, um das Nickelcermet zu erhalten.
3. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß die wasserlöslichen, durch Wärme zersetzlichen Zirkoniumoxid-, Yttrium- und Nickelsalze, die zur Herstellung der Lösung in der Stufe (a) verwendet werden, unter den Salzen der Carbonsäuren oder den Nitratsalzen ausgewählt sind.
4. Verfahren nach Anspruch 3, dadurch gekennzeichnet, daß die Zirkoniumoxid-, Yttrium- und Nickelsalze Zirkoniumnitratoxid, Zirkoniumacetatoxid, Yttriumacetat, Nickelnitrat und Nickelacetat sind.
5. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß die organischen Hydroxysäuren unter Citronensäure, Milchsäure, Glykolsäure, Weinsäure und Mandelsäure und die organischen Aminosäuren unter Glycin und Alanin ausgewählt sind.
6. Verfahren nach Anspruch 5, dadurch gekennzeichnet, daß die Hydroxysäure Citronensäure ist.
7. Verfahren nach einem der Ansprüche 2 bis 6, dadurch gekennzeichnet, daß in der Stufe (a) eine wäßrige Lösung

von Zirkoniumdioxid-, Yttrium- und Nickelsalzen in solchen Verhältnissen der Salze zueinander hergestellt wird, um in dem als Endprodukt erhaltenen Nickelcermet einen Gehalt von 35 bis 70 Gew.-% Nickelmetall und von 65 bis 30 Gew.-% Zirkoniumdioxid, stabilisiert mit 5 bis 20 Mol Yttriumdioxid je 100 Mol Zirkoniumdioxid, zu haben, wobei die Menge der organischen Hydroxysäure oder Aminosäure im Bereich von 2 bis 4 Mol je Mol Zirkonium-, Yttrium- und Nickelmetalle liegt und der pH-Wert der Lösung im Bereich von 2 bis 5 liegt.

8. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß in der Stufe (b) das Wasser aus der Lösung unter Vakuum bei einer Temperatur nicht über etwa 80°C oder durch Sprühtrocknung entfernt wird.
9. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß in der Stufe (c) die Calcinierung bei einer Temperatur im Bereich von 800°C bis 1000°C während 1 bis 10 Stunden in einer Sauerstoff-, Luft- oder mit Sauerstoff angereicherten Luftatmosphäre durchgeführt wird.
10. Verfahren nach Anspruch 9, dadurch gekennzeichnet, daß die Calcinierung bei etwa 900°C während 3 bis 5 Stunden durchgeführt wird.
11. Verfahren nach Anspruch 2, dadurch gekennzeichnet, daß in der Stufe (d) die Reduktion durchgeführt wird, indem das calcinierte feste Material mit Wasserstoffgas bei Arbeitstemperaturen im Bereich von 20°C bis 1000°C in Kontakt gebracht wird.
12. Verwendung des Nickelcermets nach Anspruch 1 als anodisches Material für Festoxid-Brennstoffzellen (SOFC solid oxide fuel cells).

Revendications

1. Cermet de nickel, constitué de 35 à 70 % en poids d'une phase de nickel métallique et de 65 à 30 % en poids d'une phase de zircone stabilisée sous la forme cubique par de l'yttria, les deux dites phases apparaissant, lors d'une analyse de diffraction des rayons X, comme distinctes et distribuées de façon homogène à une valeur inférieure à 1 µm, et ledit cermet de nickel, lorsqu'il est soumis à un essai de chimisorption d'hydrogène au moyen de la technique par impulsions, présentant un pourcentage de dispersion du nickel allant de 0,2 à 2,0 et une aire spécifique comprise dans l'intervalle allant de 2 à 12 m²/g de nickel et de 1 à 4 m²/g de cermet.
2. Procédé pour préparer le cermet de nickel selon la revendication 1, caractérisé en ce que ledit procédé comprend les étapes suivantes :
 - (a) préparation d'une solution aqueuse contenant un sel de zirconyle, d'yttrium et de nickel soluble dans l'eau et décomposable à la chaleur, et un hydroxyacide ou acide aminé organique, ou un acide polyacrylique ;
 - (b) élimination de l'eau de la solution préparée dans l'étape (a) ci-dessus, en l'absence ou pratiquement en l'absence de phénomènes de décomposition, afin de séparer un matériau solide poreux ;
 - (c) calcination du solide poreux séparé dans l'étape (b), dans des conditions oxydantes, afin de provoquer l'apparition de la formation d'un matériau solide contenant deux phases distinctes d'oxyde de nickel et de zircone stabilisée sous la forme cubique avec de l'yttria et ayant une distribution de phases d'une valeur inférieure à 1 µm ; et
 - (d) réduction de l'oxyde de nickel en nickel métallique, à l'intérieur du matériau solide obtenu dans l'étape (c), afin d'obtenir le cermet de nickel.
3. Procédé selon la revendication 2, caractérisé en ce que les sels de zirconyle, d'yttrium et de nickel solubles dans l'eau et décomposables à la chaleur, utilisés pour former la solution dans l'étape (a), sont choisis parmi les sels carboxylates et nitrates.
4. Procédé selon la revendication 3, caractérisé en ce que lesdits sels de zirconyle, d'yttrium et de nickel sont le nitrate de zirconyle, l'acétate de zirconyle, l'acétate d'yttrium, le nitrate de nickel et l'acétate de nickel.
5. Procédé selon la revendication 2, caractérisé en ce que les hydroxyacides organiques sont choisis parmi l'acide citrique, l'acide lactique, l'acide glycolique, l'acide tartrique et l'acide mandélique, et les acides aminés organiques sont choisis parmi la glycine et l'alanine.

6. Procédé selon la revendication 5, caractérisé en ce que l'hydroxyacide utilisé est l'acide citrique.
7. Procédé selon les revendications 2 à 6, caractérisé en ce que, dans l'étape (a), une solution aqueuse de sels de zirconyle, d'yttrium et de nickel est préparée avec des rapports relatifs desdits sels tels que le cermet de nickel obtenu en tant que produit final ait une teneur en nickel métallique allant de 35 à 70 % en poids et une teneur en zircon stabilisée avec 5 à 20 moles d'yttria pour 100 moles de zircon, allant de 65 à 30 % en poids, la quantité d'hydroxyacide ou d'acide aminé organique étant comprise dans l'intervalle allant de 2 à 4 moles par mole de zirconium, d'yttrium et de nickel métalliques, et le pH de la solution étant compris dans l'intervalle allant de 2 à 5.
8. Procédé selon la revendication 2, caractérisé en ce que, dans l'étape (b), l'eau est éliminée de la solution par traitement sous vide à une température ne dépassant pas environ 80°C, ou bien par séchage par pulvérisation.
9. Procédé selon la revendication 2, caractérisé en ce que, dans l'étape (c), la calcination est réalisée à une température comprise dans l'intervalle allant de 800°C à 1000°C, pendant une durée allant de 1 à 10 heures et dans une atmosphère d'oxygène, d'air ou d'air enrichi en oxygène.
10. Procédé selon la revendication 9, caractérisé en ce que ladite calcination se déroule à environ 900°C et pendant une durée allant de 3 à 5 heures.
11. Procédé selon la revendication 2, caractérisé en ce que, dans l'étape (d), la réduction se déroule par mise en contact du matériau solide calciné avec de l'hydrogène gazeux, la température de traitement étant comprise dans l'intervalle allant de 20°C à 1000°C.
12. Utilisation du cermet de nickel selon la revendication 1 en tant que matériau d'anode pour des piles à combustible de type oxyde solide (SOFC).